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1 **Ammonium acetate supplement strategy for enhancement of chaetominine**
2 **production in liquid culture of marine-derived *Aspergillus fumigatus* CY018**

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18 **Abstract**

19 Chaetominine (CHA), a marine-derived quinazolinone alkaloid with significant
20 cytotoxic activity, is restricted by low yields on pharmacological research, which needs to be
21 settled urgently. In this work, the selection of additional nitrogen sources, optimization of the
22 addition concentration and addition time of ammonium acetate, were investigated. CHA
23 production was optimized to 62.1 mg/L with the addition of 50 mM ammonium acetate at 120
24 h of the fermentation in the shaker flask. This feeding strategy significantly increased
25 3-deoxy-arabino-heptulosonate-7-phosphate synthase activity and transcript levels of critical
26 genes (*laeA*, *dahp* and *trpC*) in the shikimate pathway compared with the non-treatment group.
27 In addition, the selection of feeding rate (0.01 and 0.03 g/L/h) was investigated in a 5-L
28 bioreactor. And, CHA production was increased 57.9 mg/L with a 0.01 g/L/h ammonium
29 acetate feeding rate. This work showed the strategy of ammonium acetate supplement had an
30 effective role in improving CHA production by *Aspergillus fumigatus* CY018. This strategy
31 could provide a precious experience for the large-scale fermentation of marine fungus in
32 submerged culture.

33
34 **Key words:** Chaetominine; Marine-derived fungus; Ammonium acetate; feeding strategy;
35 *Aspergillus fumigatus*

36 1. Introduction

37 Marine resources have received the attention of many scholars owing to the abundance of
38 bioactive compounds with unique chemical structures by marine organisms [1-2].
39 Marine-derived microorganism, a renewable, prolific and efficient source, produces various
40 secondary metabolites with remarkable bioactivities, such as antitumor, antibacterial, and
41 anti-inflammatory effects [3-4]. However, the research and development of secondary
42 metabolites within a distinct framework in the pharmacodynamics field are seriously limited
43 by the low yield [5-6]. Therefore, effective biotechnological strategies imminently need to be
44 exploited for enhancing the production of target compounds by the fermentation of marine
45 microbes.

46 Many of secondary metabolites from marine symbiotic microbes possess excellent
47 bioactivity and some have been developed into drugs for the treatment of various diseases
48 [7-8]. *Aspergillus fumigatus* CY018, a symbiotic fungus of sea-crab, produces many valuable
49 metabolites with antifungal, anticancer and cytotoxic activities [9-10]. Chaetominine (CHA),
50 isolated and identified from *A. fumigatus* CY018, is a quinazolinone alkaloid (Fig. 1) with
51 significant anticancer activity against the human leukemia K562 and colon cancer SW1116
52 cell lines. Yao and co-workers found the mechanism that CHA treatment induced apoptosis in
53 human leukemia K562 cells via the mitochondrial pathway [11-12]. However, an effective
54 regulation strategy for improving the production of CHA is not available thus far, which limits
55 further research about the pharmacology and pharmacodynamic mechanism of the anticancer
56 activity of CHA.

57 The supplement of medium components as a significantly effective strategy was widely

58 applied in the fermentation process for enhancing production of target metabolites. The
59 nitrogen source as an important nutritional component affects the growth of microorganisms
60 and synthesis of secondary metabolites [13]. On one hand, the effect of limiting nitrogen
61 source can improve the production of secondary metabolites. As Wang et al. found the
62 limitation of ammonium sulfate in culture medium could improve the production of pullulan
63 by *Aureobasidium pullulans* [14]. On the other hand, the supplement of nitrogen source can
64 also effectively promote the biosynthesis of target compounds. For instance, the feeding
65 strategy of nitrogen source was beneficial for cell growth and curdlan production during the
66 early fermentation stage of *Rhizobium radiobacter* [15].

67 CHA is speculated to be biosynthesized via the shikimate pathway in the previous work.
68 Although the detailed polymerization of alanine, anthranilic acid and tryptophan is unclear,
69 the early steps of CHA biosynthetic pathway were verified as involving the shikimate
70 pathway in our previous work [16]. There are some key sites for control in the shikimate
71 pathway, such as 3-deoxy-arabino-heptulosonate-7-phosphate synthase (DAHP, *dahp*),
72 chorismate synthase (*cs*) and anthranilate synthase (*trpC*) [17-19]. In addition, *laeA*, a global
73 regulator, plays an important regulation role in the biosynthesis of secondary metabolites,
74 such as the effect of deletion/overexpression of *laeA* in *Aspergillus* spp. [20]. Thus, the
75 transcriptional expression of these key genes, *laeA*, *dahp*, *cs* and *trpC*, might have a
76 promoting role in the biosynthesis of CHA by feeding nitrogen source strategy. And, the
77 transcript levels of critical genes are verified to enhance the production of target compounds
78 [21-22]. For example, limiting glutamine (a nitrogen source) improves the transcriptional
79 expression of important related genes and the yield of ganoderic acids in *Ganoderma lucidum*

80 [23].

81 **Feeding nutrient** in the culture broth is a **usual** strategy for **enhancement of** the target
82 compounds during fermentation, especially **nitrogen source**. Moreover, Zhang et al. found the
83 optimization of nitrogen sources **significantly influences** CHA biosynthesis. Although the
84 concentration of nitrogen source was optimized in the **previous** work [24], the CHA
85 production was still low and this problem urgently requires **solving**.

86 In the **present** work, the **supplement effect** of different nitrogen sources in the broth was
87 first investigated. Then, the optimal concentration **and time** of feeding ammonium acetate
88 were determined in the shake flask. Metabolic parameters (dry cell weight (DCW), residual
89 sugar, CHA production and the activity of DAHP synthase) and **transcript** levels of **critical**
90 genes (*laeA*, *dahp*, *cs*, and *trpC*) were detected **with** the optimal fermentation condition.
91 Furthermore, the **different** feeding rate of ammonium acetate was **studied** in a 5-L bioreactor.
92 The results of this work are valuable for enhancing the production of a target compound by
93 feeding nutrient in submerged fermentation.

94

95 **2. Materials and methods**

96 *2.1. Microorganism*

97 The CHA **producing by** *A. fumigatus* CY018 utilized in this work was kindly provided
98 by Nanjing University (Nanjing, China). Mycelia were first cultured on potato dextrose agar
99 (PDA) medium for seven days at 28°C **in the constant temperature incubator** then
100 sub-cultured monthly [25].

101 *2.2. Fermentation conditions*

102 A 1.0 cm² agar tablet was cut from **cultivated** PDA and transferred to a 500 mL **shake**

103 flask containing 200 mL potato dextrose broth (PDB). After inoculation, the flask was
104 cultured as seeds at 180 rpm, 28°C, for 72 h in the oscillating constant temperature shaker.
105 Then, a 250 mL shake flask with 50 mL fermentation medium was inoculated with 7 mL of
106 seeds for culturing at 180 rpm, 28°C, for 336 h in the oscillating constant temperature shaker.
107 The fermentation medium composed of (g/L): sucrose, 100; ammonium acetate, 5; sodium
108 tartrate, 2; sodium glutamate, 2.4; KH₂PO₄, 1.2; MgSO₄·7H₂O, 0.84; and FeSO₄·7H₂O, 0.016.

109 2.3. Optimization of the nitrogen source

110 The effects of different nitrogen sources (ammonium sulfate, ammonium chloride, and
111 ammonium acetate) with 5 and 10 mM concentration at 120 h of fermentation on CHA
112 production and DCW were investigated. The effects on CHA production and DCW with
113 ammonium acetate were further examined with different concentrations (5, 10, 20, 50, and
114 100 mM) at 120 h during the fermentation. Then, ammonium acetate (screened concentration)
115 was supplied at 72, 120, 168, 216, 264 and 312 h in fermentation process, respectively. The
116 non-treatment groups were performed in cultivation medium without addition of ammonium
117 acetate.

118 2.4. Sampling and analyse

119 At the end of the fermentation process, DCW was determined to analyze the biomass of
120 *A. fumigatus*. The anthrone-sulfuric acid method was utilized to measure the residual sugar of
121 fermentation broth at different detection time. High performance liquid chromatography was
122 used to assay the content of CHA in the broth as described by Liu et al. [26]. One milliliter of
123 broth was centrifuged and the underlying mycelium was analyzed for the activity of a key
124 enzyme DAHP synthase in the shikimate pathway. The analysis method of DAHP synthase

125 was quoted by the published articles [16]. After the reaction was end, the final solution was
126 determined by measuring the decrease of PEP with spectrophotometer at 549 nm.

127 2.5. Measurement of the expression of key enzyme genes by the quantitative reverse 128 transcription polymerase chain reaction (qRT-PCR)

129 The TRIzol solution was employed to extract total RNA of taken samples for all
130 experiments. The RNA concentrations in the taken samples were determined using a
131 spectrophotometer at $A_{260/280}$. The method of Li et al. was utilized to detect mRNA expression
132 levels of *laeA*, *dahp*, *cs*, *trpC* and actin [27]. Total RNA served as the initial template and the
133 PremixScript™ Reagent Kit (Takara Bio, Kusatsu, Japan) was used for reverse transcription.
134 Premix Ex Taq™ II (Takara Bio) was utilized to determine mRNA levels of key genes
135 according to the manufacturer's procedure. Primer pair sequences for qRT-PCR amplification
136 of *laeA*, *dahp*, *cs*, *trpC*, and actin are displayed in Table 1. The qRT-PCR was performed as
137 displayed by the published paper [16].

138 2.6. Batch-fed fermentation in a 5-L bioreactor

139 The research of feeding flow rate with ammonium acetate was worthy in the bioreactor.
140 The feeding flow rates of ammonium acetate (0.01 g/L/h, 0.03 g/L/h and non-treatment) on
141 batch-fed fermentation were investigated in a 5-L stirred bioreactor. A 1 L shake flask
142 containing 400 mL PDB was cultured on shaker at 180 rpm, 28°C, for 72 h in the oscillating
143 constant temperature shaker. Then, this was inoculated into the bioreactor containing 2.6 L
144 medium and fermented for 384 h at $28 \pm 0.2^\circ\text{C}$ with a stirring speed of 300 rpm. Air flow was
145 controlled at 1.5 ± 0.1 vessel volume/min during the fermentation process. Antifoam (a
146 mixture of organic polyether dispersions) was added at 0.3% (v/v) before autoclaving.

147 Fermentation broth (20 mL) was taken at intervals of 48 h for detecting the metabolic
148 parameters.

149 *2.7. Statistical analyse*

150 All experiments in the shake flasks were performed in triplicate. Error bars in the figures
151 indicate the corresponding standard deviations. A value of $P < 0.05$ was considered
152 statistically significant. Origin 8 software (OriginLab, Northampton, MA, USA) was utilized
153 to create the figures and CFX Manager (Bio-Rad, Hercules, CA, USA) was used to analyze
154 the qRT-PCR data.

156 **3. Results and discussion**

157 *3.1. Effects of adding different nitrogen sources*

158 **Nutrients in the culture broth, especially nitrogen sources,** played important roles in the
159 biosynthesis of secondary metabolites. Moreover, Zhang et al. discovered that the effects of
160 **different nitrogen sources and concentrations** on CHA production were obviously significant
161 [24]. **However, the production of CHA was also at a low level.** Therefore, we fed the
162 supernumerary nitrogen source for enhancement of CHA production. **The effects of feeding 5**
163 **and 10 mM** three different nitrogen sources (ammonium sulfate, ammonium chloride, and
164 ammonium acetate) **were investigated.** As shown in Table 2, the production of CHA was 31.6
165 ± 3.1 and 25.4 ± 1.6 mg/L with 5 and 10 mM ammonium sulfate, respectively. This indicated
166 that CHA production was decreased with an increasing content of ammonium sulfate, **which**
167 **implied** that effect of ammonium sulfate addition was not significant on CHA production.

168 The production of CHA (32.5 ± 1.6 and 34.5 ± 3.2 mg/L) was **slightly** increased with 5

169 and 10 mM ammonium chloride. The highest production of CHA was 42.5 mg/L with the
170 addition of 10 mM ammonium acetate in the selection experiments, which production was
171 45.3% higher than the non-treatment group. Therefore, the addition of ammonium acetate
172 played a significantly promoting role in CHA production, suggesting that feeding ammonium
173 acetate might be an effective strategy for enhancement of CHA production.

174 3.2. Concentration-and time- effects of ammonium acetate addition on CHA production

175 Because feeding ammonium acetate was beneficial for increasing CHA production by *A.*
176 *fumigatus* CY018, the optimal concentration and time of ammonium acetate supplement were
177 investigated. As shown in Fig. 2A, the effects of different concentrations of ammonium
178 acetate (5, 10, 20, 50 and 100 mM) at 120 h were promoted CHA biosynthesis at different
179 levels. The trend of CHA production was improved when concentration of ammonium acetate
180 was increased from 5 to 50 mM. Specifically, the optimal concentration of ammonium acetate
181 was 50 mM, where CHA production reached the maximum (64.7 mg/L) which was 2.2 folds
182 compared that in non-treatment group. 100 mM concentration of ammonium acetate resulted
183 in the CHA production decreasing to 41.9 mg/L, indicated that a high content of ammonium
184 acetate had a negative effect on CHA biosynthesis. Therefore, the optimized concentration of
185 ammonium acetate supplement for enhancing CHA production was 50 mM.

186 The feeding time of ammonium acetate also played an important role in CHA
187 biosynthesis. The determinate ammonium acetate (50 mM) was added at different time of the
188 fermentation (72, 120, 168, 216, 264 and 312 h) in the shake flasks (Fig. 2B). The production
189 of CHA was first increased then decreased with feeding time, which reached a maximum
190 (62.0 mg/L) at 120 h. The promoting effect of ammonium acetate supplement on CHA

191 production at early times might be related to the beneficial effects of nutrient addition on
192 fungal growth and product synthesis [28]. Overall, the optimal condition of ammonium
193 acetate **supplement** for CHA biosynthesis was feeding 50 mM ammonium acetate at 120 h
194 after inoculation. Hence, the **supplement** of ammonium acetate was an effective strategy for
195 improving CHA production (Fig. 3).

196 *3.3. Effects of the feeding strategy on metabolic parameters*

197 The strategy of feeding ammonium acetate (50 mM at 120 h) was confirmed to have a
198 significant positive **role in** CHA biosynthesis. Thus, metabolic parameters (DCW, residual
199 sugar, CHA production, and DAHP synthase activity) were further investigated during the
200 fermentation process in shake flask.

201 As shown in Fig. 4A, the trends of DCW in the feeding ammonium acetate and
202 **non-treatment** groups were similar before 120 h culture time. Thereafter, the growth of cells in
203 the group that was fed with ammonium acetate was higher than the **non-treatment** group. The
204 maximal DCW in the test and **non-treatment** groups were 19.4 and 16.7 g/L at 288 h,
205 respectively.

206 The consumption tendency of residual sugar **continued to decline in both groups**, while
207 residual sugar was consumed quickly after feeding ammonium acetate (Fig. 4B). As shown in
208 Fig 4C, the trend of CHA production was first increased and then decreased. Moreover, CHA
209 production with the addition of ammonium acetate was 1.9 folds higher than that in
210 **non-treatment** (33.7 mg/L). **Moreover, the yield of CHA with ammonium acetate addition was**
211 **higher than non-treatment group in supplemental data 1, which meant the increasing CHA**
212 **production appeared to be in the growth-dependent manner.**

213 In previous research, we **speculated** and verified that the biosynthesis of CHA was
214 through the shikimate pathway, and that DAHP synthase was a key enzyme in the process.
215 Thus, **the activity of DAHP synthase** was investigated with ammonium acetate supplement at
216 different **taken points of** the fermentation process (Fig. 4D). **The activity of DAHP synthase**
217 increased and then decreased in both the test and **non-treatment** groups. Importantly, the
218 activity of DAHP synthase increased to a maximum, which was 52.6% above **the**
219 **non-treatment group** at 240 h. These data indicated that the strategy of ammonium acetate
220 **supplement** was beneficial for improving **the biosynthesis of CHA**.

221 Yang et al. also found that various fermentation parameters, the activities of key enzymes
222 and the **content** of metabolites were enhanced when either urea or ammonium chloride was
223 used as the sole source of nitrogen [29]. **It can clearly be seen** the strategy of feeding
224 ammonium acetate could significantly promote the activity of key enzyme to optimize
225 fermentation parameters for enhancing CHA production.

226 3.4. Gene expression in response to ammonium acetate addition

227 The feeding strategy we used **was benefited for** cell growth and DAHP synthase activity
228 **to enhance** CHA production. We next researched the **mRNA transcript** levels of *laeA*, *dahp*, *cs*
229 and *trpC* using qRT-PCR to explore the mechanism of this effective strategy. The
230 transcriptional levels of these key genes with **supplement** of ammonium acetate were taken
231 **samples** at 48, 144, 240 and 336 h during the fermentation.

232 As shown in Fig. 5A, feeding ammonium acetate significantly **increased** the expression
233 of *laeA* 4.2 fold and 2.4 fold at 144 and 336 h, respectively, compared to the **non-treatment**
234 **group**. The **mRNA transcript levels** of *dahp* were also improved remarkably (43.4 fold and

235 5.5 fold at 144 and 240 h, respectively) with **supplement** of ammonium acetate (Fig. 5B).
236 The trend of *trpC* expression was similar to the **formers** (Fig. 5D). In contrast, the influence
237 of ammonium acetate addition was not significant on **mRNA transcript** level of *cs* (1.5- and
238 1.3- folds increases at 144 and 336 h, respectively) (Fig. 5C). These **results** demonstrated the
239 **supplement** of ammonium acetate could promote the **mRNA transcript** expression of key
240 genes in the CHA synthesis pathway.

241 In general, an effective strategy for enhancing **production of** target compound **could affect**
242 mRNA or protein levels of regulated factors in the biosynthesis pathway of target compound.
243 For example, Lu et al. found the biosynthesis of dalesconols A and B was enhanced via
244 calcium/calmodulin signaling with addition of Ca^{2+} [30]. In addition, Long et al. demonstrated
245 that **production of** cellulase and hemicellulase was improved via the **increased** transcription
246 factor, *creA*, in *Trichoderma orientalis* EU7-22 [31]. **Moreover**, Pandey and co-workers found
247 that vindoline production was promoted by up-regulation of the Catharanthus AP2-domain
248 protein and down-regulation of Cys2/His2-type zinc finger protein family transcriptional
249 repressors [32].

250 We researched the **mRNA transcript levels** of important genes/enzymes for **revealing** the
251 effect of our strategy on CHA production. In the current work, feeding ammonium acetate
252 **increased** the transcription levels of *laeA*, *dahp* and *trpC*, which were key genes involved in
253 DAHP synthase activity and CHA production. The activity of DAHP synthase was also
254 **improved** by the feeding strategy. This meant **supplement of** ammonium acetate positively
255 regulated gene expression to improve enzyme activity. Therefore, the obtained **results** showed
256 and verified that the strategy of ammonium acetate **supplement** up-regulated the transcription

257 levels of key genes in the biosynthetic pathway to promote the biosynthesis of CHA by *A.*
258 *fumigatus* CY018.

259 3.5. Ammonium acetate feeding strategy in a 5-L bioreactor

260 The **feeding rate of nutrient** is a helpful strategy in scale-up fermentation. Zhang et al.
261 found that feeding glucose was beneficial for Antrodin C accumulation with **40 g/L glucose** in
262 a 15-L bioreactor [33]. Therefore, for scaling up the fermentation with feeding ammonium
263 acetate, the feeding rate (0.01 and 0.03 g/L/h) was investigated in a 5-L stirred bioreactor
264 compared to **non-treatment** (Fig. 6C). The time profiles of dissolved oxygen (DO), residual
265 sugar, CHA production, DCW, and pH were first investigated with the feeding rate of 0.03
266 g/L/h (Fig. 6A).

267 The trend of DO was similar to **non-treatment** but decline slowly and maintained 0 from
268 216-312 h. Cell growth and CHA biosynthesis resulted in DO declining and cell death
269 resulted in the DO rebound. DCW was also similar to **non-treatment** and the value of DCW
270 with addition was higher than control. Residual sugar in the 5-L bioreactor was consumed
271 rapidly compared to **non-treatment** and finally reached 11.3 g/L. CHA production in the 5-L
272 bioreactor was increased to the maximum value of 46.99 mg/L at 312 h and then decreased.
273 CHA concentration decreased towards the end of the fermentation which indicated metabolic
274 instability for the target secondary metabolite. One known example of this was clavulanic
275 acid [34-35]. The phenomenon demonstrated a novel routes in fermentations would be open
276 to lead to the product of CHA decrease. The pH increased early during the fermentation
277 process, then decreased and remained at approximately 4.0 earlier than **non-treatment**. This
278 pH was beneficial to cell growth and target compound synthesis.

279 CHA production in the 5-L bioreactor with a 0.03 g/L/h feeding rate was lower than the
280 results in the shake flasks (62.10 mg/L). This indicated that the rate of feeding ammonium
281 acetate needed to be adjusted. A 0.01 g/L/h rate of feeding ammonium acetate was applied in
282 the 5-L bioreactor (Fig. 6B). DO, residual sugar, and pH were all increased for a short time
283 (96-144 h) after feeding, which were similar to **non-treatment**. The trend of DCW was greater
284 the 0.03 g/L/h rate. Moreover, CHA production reached 57.9 mg/L, which was more close to
285 the 62.10 mg/L in the shake flask than 0.03 g/L/h rate and **non-treatment** (46.11 mg/L). This
286 information meant that a 0.01 g/L/h rate of feeding ammonium acetate was more beneficial
287 for CHA biosynthesis than a 0.03 g/L/h rate and **non-treatment** in the 5-L bioreactor.
288 **Moreover, the detail comparison of each parameter (DO, residual sugar, chaetominine**
289 **production, DCW, and pH) was shown in the supplemental data 2.**

290 Hence, the fermentation of *A. fumigatus* CY018 for producing CHA was successfully
291 **scaling-up** with feeding 0.01 g/L/h rate ammonium acetate in 5-L bioreactor. The results of
292 the current work indicated that the **supplement** strategy of ammonium acetate was beneficial
293 for CHA biosynthesis by *A. fumigatus* CY018. Meanwhile, this provided a **valuable**
294 experience for enhancing target compound production in submerged fermentation.

295 Finally, in this paper, the supplement of selected ammonium acetate was beneficial for
296 CHA biosynthesis. **The optimization of addition concentration and time** of ammonium acetate
297 was first performed in the shake flask. Maximal CHA production (62.1 mg/L) was achieved
298 with addition of 50 mM ammonium acetate at 120 h **of fermentation**. The **activity of key**
299 **enzyme** and transcription levels of key genes (*laeA*, *dahp* and *trpC*) were promoted with
300 **supplement strategy of** ammonium acetate, which enhanced CHA production ultimately.

301 Moreover, the feeding rate of ammonium acetate was researched and determined to be 0.01
302 g/L/h in 5-L bioreactor. These results demonstrated that **supplement of** ammonium acetate
303 was a significant strategy to improve the production of CHA. Furthermore, this work
304 provided a **precious** experience for promoting target compound from marine fungus by
305 **supplement of** effective nutrients in submerged fermentation.

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312 **Compliance with Ethical Standards**

313 **Conflict of Interest**

314 The authors declare that they have no conflict of interest.

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420 **Figure Captions**

421 **Fig. 1** Chemical structure of chaetominine.

422 **Fig. 2** Effects of addition concentration (A) and addition time (B) of ammonium acetate on
423 chaetominine (CHA) production and dry cell weight (DCW) at 336 h (180 rpm, 28 °C) by
424 *Aspergillus fumigatus*. Non-treatment group: without addition of ammonium acetate.
425 Experimental of addition concentration: 5, 10, 20, 50 and 100 mmol/L. Experimental of
426 addition time: 72, 120, 168, 216, 264 and 312 h. * Indicates statistical significance ($P < 0.05$)
427 compared to the control group.

428 **Fig. 3** HPLC chromatograms of CHA at 227 nm in the non-treatment group and ammonium
429 acetate supplement group (50 mmol/L, 120 h) at 336 h (180 rpm, 28 °C) by *Aspergillus*
430 *fumigatus*. Condition of HPLC: acetonitrile: water = 65: 35, flow = 1 mL/min, temperature =
431 25 °C, injection volume = 20 µL.

432 **Fig. 4** Time courses of DCW (A), residual sugar (B), chaetominine production (C) and DAHP
433 synthase activity (D) in shake flask with non-treatment and ammonium acetate feeding
434 strategy. *Aspergillus fumigatus* CY018 was cultured 360 h at 180 rpm and 28 °C. * Indicates
435 statistical significance ($P < 0.05$) compared to the non-treatment group.

436 **Fig. 5** Response of transcript level of genes related to chaetominine biosynthesis when
437 feeding strategy and non-treatment were shown. *laeA* as a global regulator (A), *dahp* as
438 3-Deoxy-arabino-heptulosonate-7-phosphate synthase (B), *cs* as chorismate synthase (C), and
439 *trpC* as anthranilate synthase (D). *Aspergillus fumigatus* CY018 was cultured 360 h at 180
440 rpm and 28 °C. * Indicates statistical significance ($P < 0.05$) compared to the non-treatment
441 group.

442 **Fig. 6** Time courses of DO, chaetominine production, residual sugar, pH, and DCW in
443 *Aspergillus fumigatus* cultured in 5-L bioreactor with feeding rate of 0.03 g/L/h (A), 0.01
444 g/L/h (B) and non-treatment (C) The culture condition of *A. fumigatus* CY018 was 300 rpm,
445 28 °C and 1.5 ± 0.1 vessel volume/min of air flow. The 11.55 g of ammonium acetate (50 mM,
446 3 L broth) was supplied at 120 h.

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448 **Table Captions**449 **Table 1.** Sequences of primer pairs for quantitative real-time RT-PCR (qRT-PCR) assay.

Target gene	Primer name	Primer sequence (5'-3')
<i>laeA</i>	<i>laeA</i> -forward	TTC TTTCGAGCTGCCG TCAA
	<i>laeA</i> -reverse	TCCATGGTATGTTTCGTCCGT
<i>dahp</i>	<i>dahp</i> -forward	GACAAGGGCCCATCTTCACA
	<i>dahp</i> -reverse	TGGCAGACGTGTTATAGCGG
<i>cs</i>	<i>cs</i> -forward	CCCCCGAACAATGAATCGC
	<i>cs</i> -reverse	GGTACTTCTCCGCAATGGCT
<i>trpC</i>	<i>trpC</i> -forward	AGGTCGACGTTTTTCGGTGAA
	<i>trpC</i> -reverse	AGTCACTTCAACCGCAGGAG
<i>actin</i>	<i>actin</i> -forward	TTCGAGACCTTCAACGCTCC
	<i>actin</i> -reverse	ATGGGGACAACGTGAGTGAC

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451 **Table 2.** Effect of different nitrogen sources addition on CHA biosynthesis. * Indicates
452 statistical significance ($P < 0.05$) compared to the **non-treatment** group.

Nitrogen source	Dry cell weight (g/L)	Production of CHA (mg/L)
Non-treatment group	21.98 ± 1.60	29.27 ± 3.04
5 mM ammonium sulfate	19.43 ± 2.04	31.62 ± 3.05
10 mM ammonium sulfate	19.46 ± 1.99	25.35 ± 1.55
5 mM ammonium chloride	20.53 ± 1.27	32.52 ± 2.11
10 mM ammonium chloride	20.61 ± 1.28	34.54 ± 3.17
5 mM ammonium acetate	20.47 ± 1.13	32.73 ± 1.25
10 mM ammonium acetate	21.83 ± 2.11	42.52 ± 2.26*

453

1 **Ammonium acetate supplement strategy for enhancement of chaetominine**
2 **production in liquid culture of marine-derived *Aspergillus fumigatus* CY018**

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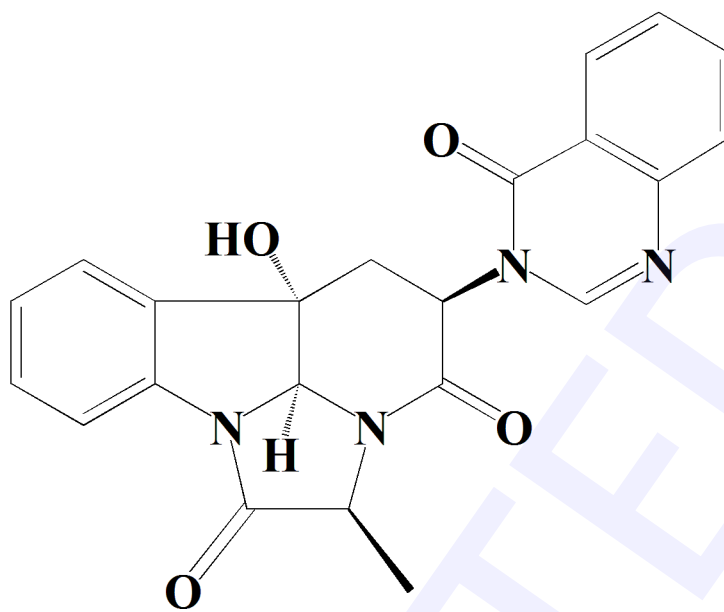
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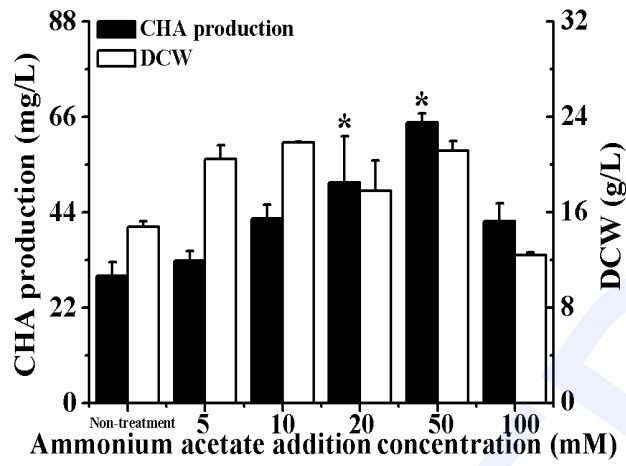
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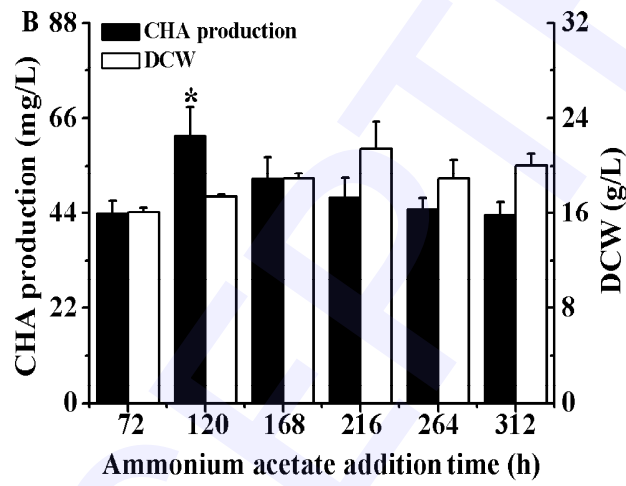
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Fig. 1

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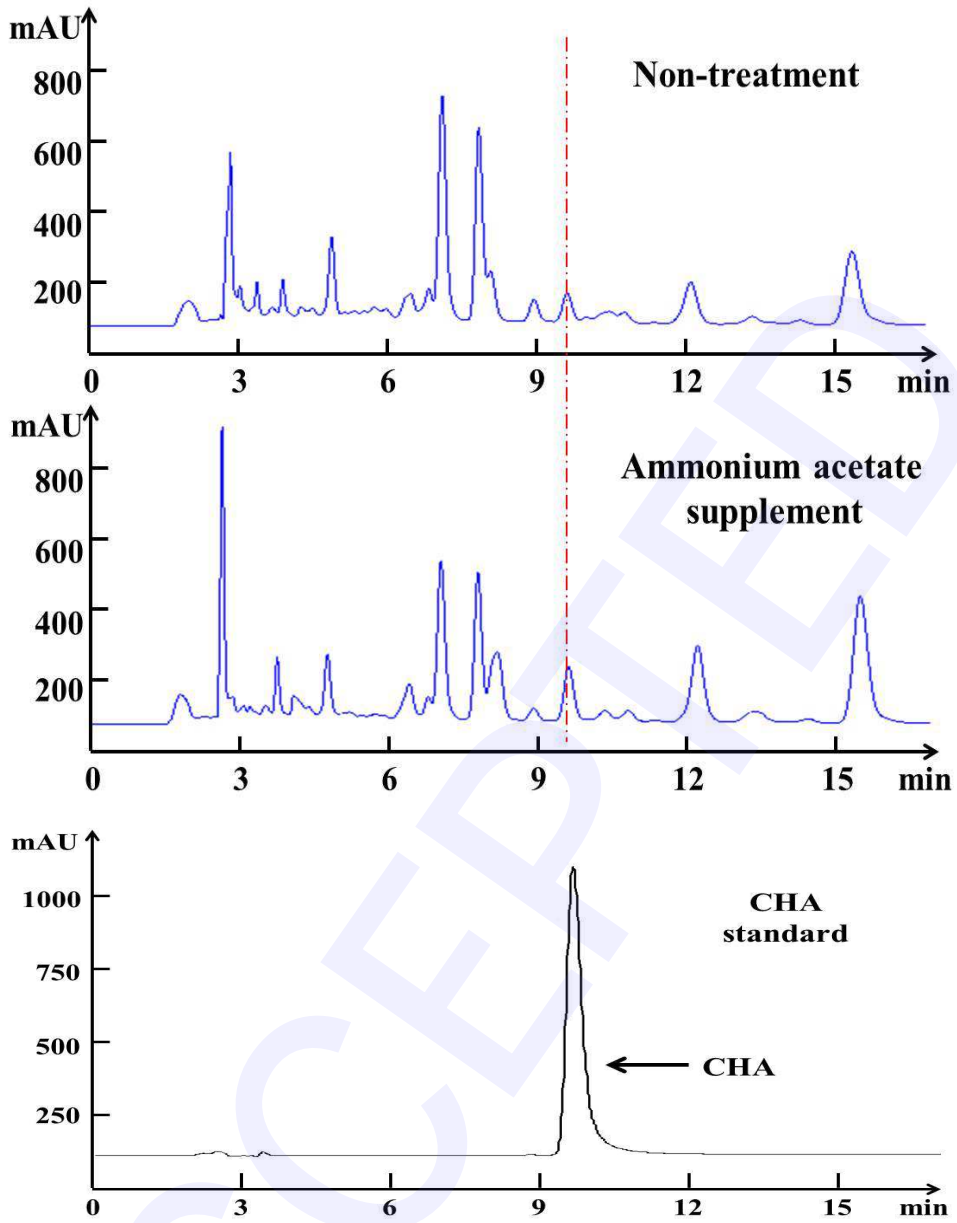


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Fig. 2

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Fig. 3

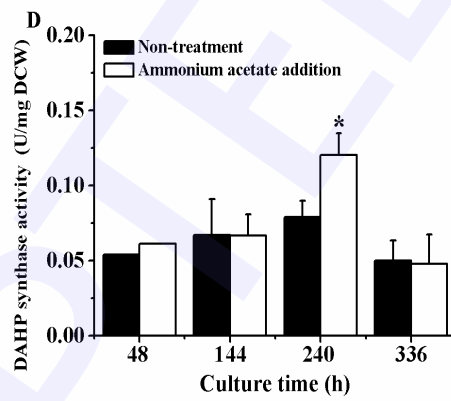
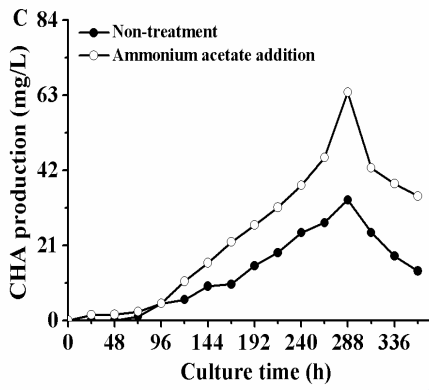
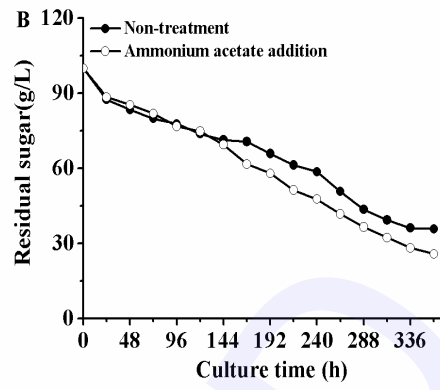
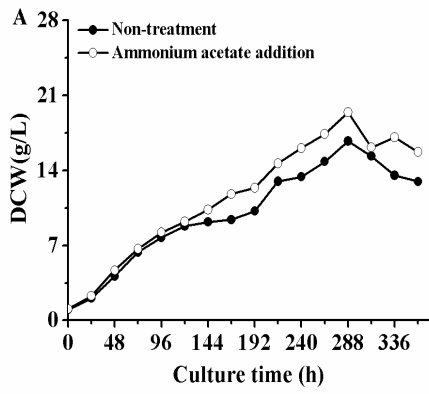


Fig. 4

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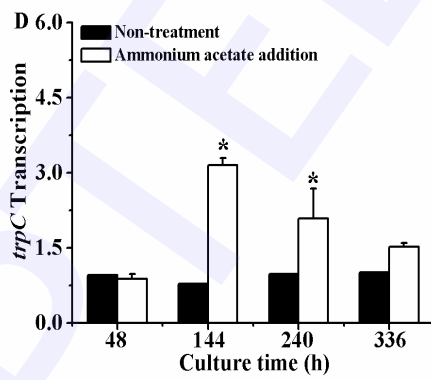
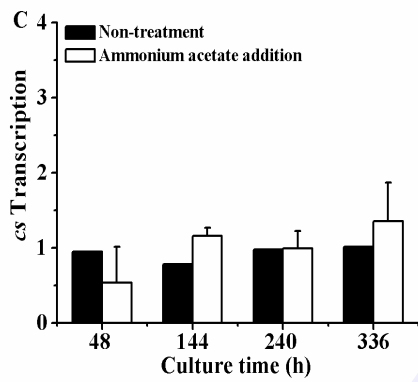
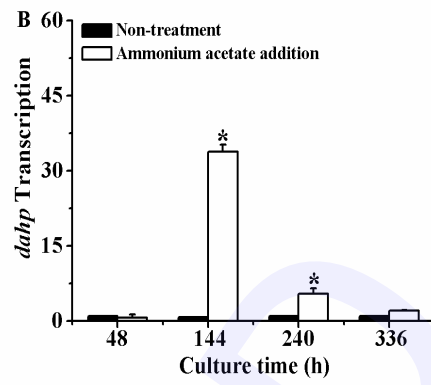
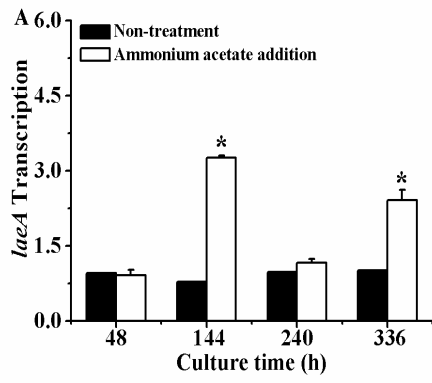


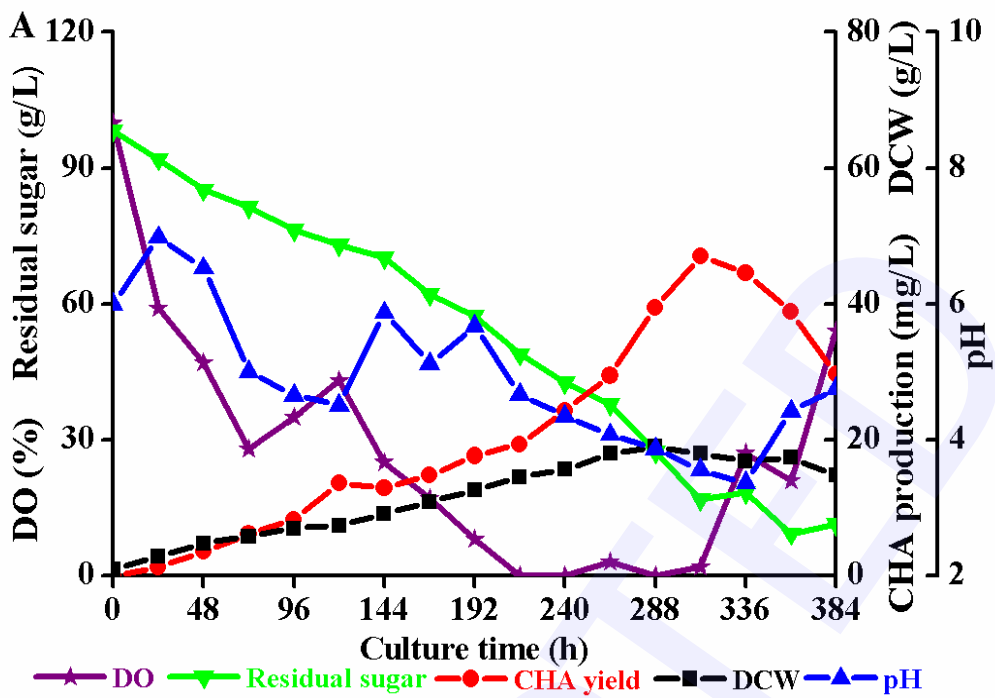
Fig. 5

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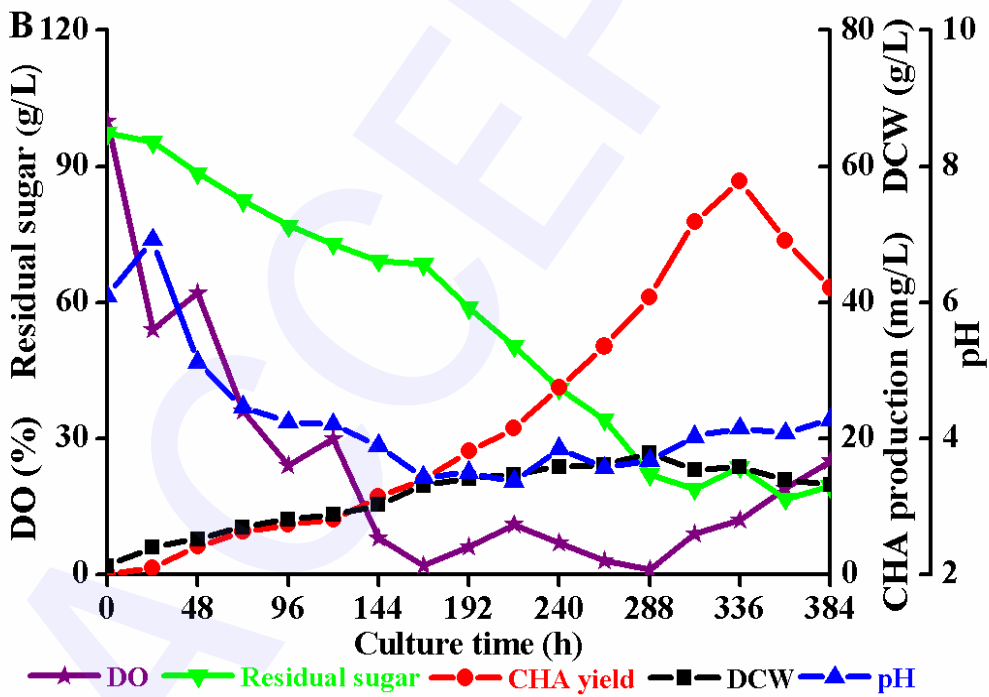
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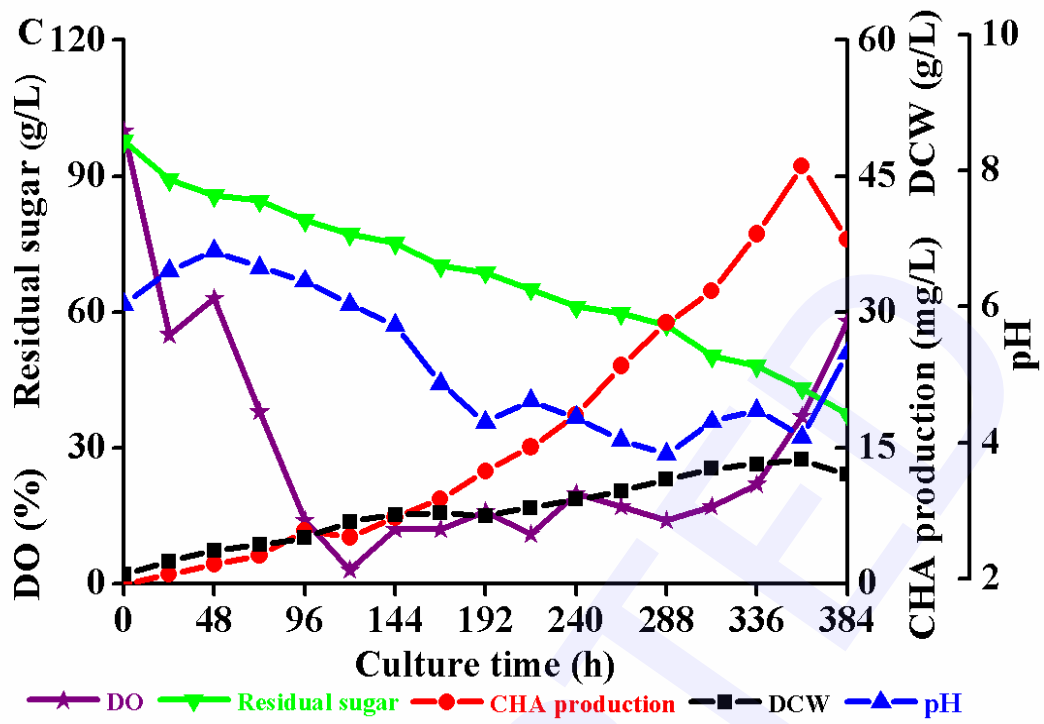


Fig. 6

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